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The data and conclusions presented here are for the use of the personnel of the Naval Ordnance Laboratory. They may not represent the final judgment of the Laboratory.

Refr:

- Kilnc-Thompson: "Theoretical Hydrodynamics", Macmillan, Chapters 11, 12.
- Kreisel, G.: "Cavitation with Finite Cavitation Numbers", Admiralty Research Laboratory Report.
- Kiabouchinski, D.: "Sur les singularites des mouvements fluides", Proceedings of the Second International Congress for Applied Mechanics, pp. 512-518.

Encl:

- (HW) Figures 1 through 4.
- (HW) Tables I and II.

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It is well known that the flow of a liquid past a body is characterized by a velocity in the region of the body. The velocity of the flow is denoted by V . The pressure in the liquid is denoted by p . The density of the liquid is denoted by ρ . The dynamic pressure is denoted by $\frac{1}{2}\rho V^2$. The static pressure is denoted by p_s . The total pressure is denoted by p_t . The pressure coefficient is denoted by C_p . The cavitation number is denoted by K . The cavitation number is defined as $K = \frac{p_s - p_v}{\frac{1}{2}\rho V^2}$, where p_v is the vapor pressure of the liquid.

The cavitation number is a dimensionless quantity which characterizes the extent of cavitation. It is defined as the ratio of the static pressure to the dynamic pressure, minus the ratio of the vapor pressure to the dynamic pressure. In water tunnel experiments, the cavitation number is reduced by letting p approach p_v in water entry experiments, the dynamic head is controllable, so that $\frac{1}{2}\rho V^2$ can be made as small as desired.

$$K = \frac{p_s - p_v}{\frac{1}{2}\rho V^2}$$

The size of the cavity increases as K approaches zero, that is, as p approaches p_v or as $\frac{1}{2}\rho V^2$ approaches zero. In water tunnel experiments, there are limitations on the maximum attainable velocity V , the cavitation number is reduced by letting p approach p_v in water entry experiments, the dynamic head is controllable, so that $\frac{1}{2}\rho V^2$ can be made as small as desired.

3. The theory of the cavity formed when the static pressure in the liquid is equal to the pressure in the cavity is identical in the two-dimensional case with the theory of the infinite wake (Figure 1-a) which was first explored by Kirchhoff and Helmholtz, and later extended by Levi-Civita and others; see reference (a) for some details of this work. Physically the infinite cavity cannot occur, but can be considered as the limiting case of what occurs as the dynamic head increases without limit relative to the static pressure in the undisturbed liquid, or as the static pressure approaches the cavity pressure.

4. The Kirchhoff flow is limited to infinite cavities and zero cavitation number. An exact theory of the finite cavity corresponding to non-zero cavitation number has only recently been given. This theory is attributed to H. Wagner, although unpublished by him, and was developed independently in 1945 by G. Kreisel of the Admiralty Research Laboratory, England (reference 1). The essential feature of the theory is the occurrence of a reverse jet extending from the rear of the cavity through the obstacle to infinity, as shown in Figure 1-b. Although this seems physically objectionable, it is a good description of what has been observed experimentally at the Naval Ordnance Laboratory. Jets do indeed occur in finite cavities, although they are either weakened by the turbulent mixing at the rear of the cavity, or finally collide with the obstacle.

is easily seen that the flow is irrotational in that it satisfies the conditions for irrotationality. The velocity components are given by the following expressions:

$$u = \frac{\partial \phi}{\partial x} = \frac{1}{2} \left(\frac{P-p}{\rho V^2} \right) \left(1 - \frac{y^2}{x^2} \right)$$

$$v = \frac{\partial \phi}{\partial y} = \frac{1}{2} \left(\frac{P-p}{\rho V^2} \right) \left(\frac{y}{x} \right)$$

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$$\frac{1}{2} \left(\frac{P-p}{\rho V^2} \right) \left(1 - \frac{y^2}{x^2} \right) = \frac{1}{2} \left(\frac{P-p}{\rho V^2} \right) \left(1 - \frac{y^2}{x^2} \right)$$

where U is the (constant) flow velocity in the free streamlines. Thus

$$\frac{U^2}{V^2} = \frac{P-p}{\rho V^2} + 1 = 1 + N$$

When $P = p$, and therefore $N = 0$, the classical Kirchhoff type flow shown in Figure 1-a prevails.

8. For the case $P > p$, consider the flow shown in Figure 1-b. We shall need only the upper half of the flow plane, which will be designated the z -plane. The flow problem is solved once the complex velocity potential, $w(z) = \phi + i\psi$, is determined, where ϕ is velocity potential, ψ is stream function.

- * This is required by the fact that the pressure always increases from the cavity into the flow.
- ** The following treatment can very easily be applied to wedges also.

... ..

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(1) ϕ -plane on the ξ -plane

$$\frac{dy}{dx} = \frac{K_1}{(c-c)(c-1)(c-b)^{1/2}}$$

$$K_1 = C \sqrt{B}/2 = C \sqrt{C-T} \sqrt{C-B}$$

(A) $\therefore \sqrt{C-1} \sqrt{C-5} = \sqrt{5/2}$

(2) w -plane on the ζ -plane

$$\frac{dW}{dC} = K_2 \frac{C-b}{C-a}$$

with subsidiary condition

$$K_2 = \psi_0 / \pi (c - b) \quad .$$

From (1) it follows that

$$Q = \frac{1}{2} \log \frac{\sqrt{5-b} + \sqrt{b}}{\sqrt{5-b} - \sqrt{b}} \frac{\sqrt{5-1}}{\sqrt{5-1}} + \log \frac{\sqrt{5-1} \sqrt{5-b} + \sqrt{5-b} \sqrt{5-1}}{\sqrt{5-1} \sqrt{5-b} - \sqrt{5-b} \sqrt{5-1}} + \log k$$

10. The drag is computed by integrating the excess pressure over the front face of the plate, neglecting the effect of the jet on the back face, however.

$$\frac{1}{\pi (c-b)} \int_0^{\psi_0} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right)^{1/2} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right) d\psi$$

The thickness of the jet is ψ_0/U . The shape of the cavity is given parametrically as a function of ψ ($0 \leq \psi \leq \psi_0$) by the expression

$$\frac{\psi_0}{\pi (c-b)} \int_0^{\psi} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right)^{1/2} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right) d\psi$$

and the length L of the cavity

$$L = \int_0^{\psi_0} \left(\frac{\psi_0}{\pi (c-b)} \right)^{1/2} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right) d\psi$$

$$\frac{1}{\pi (c-b)} \int_0^{\psi_0} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right)^{1/2} \left(\frac{\sqrt{c-b} \sqrt{1-\frac{\psi}{\psi_0}}}{\sqrt{1-\frac{\psi}{\psi_0}}} \right) d\psi$$

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10. The drag is computed by integrating the excess pressure over the front face of the plate, neglecting the effect of the jet on the back face, however.

$$\text{Drag} = C_D \frac{1}{2} \rho U^2 = \rho \int_0^{\psi_0} (U^2 - q^2) d\psi, \quad (C_D = \text{drag coefficient})$$

$$C_D = \frac{U^2}{U^2} \left(1 - \frac{\int_0^{\psi_0} q^2 d\psi}{\int_0^{\psi_0} U^2 d\psi} \right)$$

Since

$$\int_0^{\psi_0} q^2 d\psi = -1 \int_0^{\psi_0} \left(\frac{dq}{d\psi} \right)^2 d\psi = -1 \int_0^{\psi_0} \frac{dq}{d\psi} d\psi = 1 \int_0^{\psi_0} \frac{dq}{d\psi} d\psi$$

then

$$C_D = \frac{U^2}{U^2} (1 - L_1/L_2) = (1 + M) (1 - L_1/L_2)$$

where

where l is the integrand in the integral I_1 , z is the point of integration in the z -plane excluding the point $z = 1$, $z = 1$ is the origin. The path of integration is taken as the segment of the real axis in the z -plane (corresponding to the width of the plate in the z -plane), and the branch principal value at the point of the integral, the real part of the result is the distance between stagnation points, while the imaginary part is the thickness of the jet which corresponds to the jump at $z = 1$.*

11. The integrals in the expression for C_D can be written in terms of elementary functions. C_D was evaluated for cavitation numbers between 0 and 1.5. The curve of drag coefficient vs. cavitation number is shown in Figure 2, and is seen to be almost a straight line. The variation of l_1/l_2 with cavitation number is shown in Figure 3; over the region considered the total variation remains less than 8%. To a good approximation, it follows

$$C_D = C_{D_0} (1+N) = 0.88(1+N)$$

where $C_{D_0} = 0.88$ is the drag coefficient of a flat plate with infinite cavity and zero cavitation number, the well-known result of Kirochhoff. Table I shows the variation of the different parameters and integrals.

12. Calculations of the thickness of the jet show it to be essentially constant and equal to 22% of the plate width over the considered region of cavitation numbers.

13. The length of the cavity, which is taken to be the distance between stagnation points, is plotted in units of plate width in Figure

* The preceding analysis is contained essentially in reference (b).

the first obstacle which presents itself in the solution. In fact, the total thrust on it is equal to the force on the forward obstacle, so that the total force on the flange rivets is zero, as would be expected from the D'Alembert paradox.

$$\frac{dQ}{dt} = \frac{K_s}{(w^2 - a^2)(w^2 - b^2)^{1/2}}$$

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$$Q = K_1 \cos_3 \left[\frac{\frac{a}{\sqrt{a^2 - b^2}} + \frac{\sqrt{W^2 - E^2} + \sqrt{a^2 - b^2}}{W + a}}{\frac{a}{\sqrt{a^2 - b^2}} + \frac{\sqrt{W^2 - E^2} + \sqrt{a^2 - b^2}}{W - a}} \right]$$

The conditions

$$Q = 0 \text{ at } w = 0, \quad Q = -1\pi/2 \text{ at } w = 1$$

give $K_2 = 0$, $K_1 = -1/2$, and therefore, since $Q = \log \frac{ds}{du}$

- * Note that the distance between the plates for a flow with preassigned cavitation number is one of the unknowns of the problems. Conversely, if the position of the plates is fixed, the cavitation number is unknown.

the velocity of the fluid at the stagnation point is zero.

Let us now consider the velocity of the fluid at the stagnation point.

$$(b) \quad U_0 = \frac{1}{2} \left(\frac{1}{t} + t \right) \quad \text{where } t = \sqrt{1 - k^2}$$

where

$$(b) \quad I_1 = - \int_0^1 \left(\frac{1}{t} \right) \cdot \frac{1}{2} dt$$

$$(b) \quad I_2 = \int_0^1 \frac{1}{2} dt$$

being given by (a) above. These integrals can be expressed in terms of elliptic integrals.

$$\begin{aligned} -I_1 &= -E(k, \pi/2) - F(k, \pi/2) - (t^2 - 1) \\ I_2 &= t^2 E(k, \pi/2) - F(k, \pi/2) + (t^2 - 1) \end{aligned} \quad (k = \sqrt{1 - t^2})$$

where E and F are the complete elliptic integrals of the first and second kind, respectively.

17. The length of the cavity, which is the distance between stagnation points A, A' is given by

$$= \frac{1}{2} \frac{\int_0^1 I dw'}{\int_0^1 I dw'}$$

If the upper integral is replaced by $\int_0^1 I dw'$, the real part of the resulting expression represents the half-distance between stagnation

As shown with sufficient clarity from one another, the exact or fairly good cavity number is taken into account.

10. The evaluation of the cavity length shows a similar agreement between the two theories. The cavity lengths and elevations are tabulated in Table II in units of the plate width, and the former is plotted as a function of cavitation number in Figure 3, where it is compared with the cavity length calculated from the Wagner model. The agreement between the two theories is seen here also to be remarkably close, although deviations begin to appear at high cavitation numbers. The cavitation number, however, gives cavity length (in units of plate width) as a function of

11. The numerical agreement between these apparently dissimilar theories is not surprising, since the only significant physical difference between the two occurs at the rear portion of the cavity, where it would not be expected to affect the drag, cavity length, or other features of the flow in the large. The finite cavities observed in water-entry or water tunnel studies differ from the two models studied here chiefly in the situation at the rear of the cavity. Naturally, the portion of the converging streams of liquid at the rear stagnates and the results are a much weakened jet, or none at all, so that the physical situation is intermediate in shape between the two theoretical models. Although measurements have not been made on two-dimensional cavities to confirm the results presented here, water tunnel studies on the flow about a flat disk, in which the pressures over the face of the disk were integrated to obtain the drag, show a similar linear variation of drag coefficient. This would seem to confirm the results presented here for the corresponding two-dimensional flow.

12. Mathematical solutions do not yet exist for any three-dimensional cavity flows. The applicability of analytic methods seems to be unlikely at present. The close agreement between the simplified Riabouchinski model of the cavity and the basically correct Wagner model suggests that the former will give an accurate description of the three-dimensional cavity flow, and at the same time this model offers some

hope of successful immemorial treatment. A check against the adequacy of the theory can also be obtained from already available experimental results. From the theoretical point of view, however, the information on the frequency of the oscillations, as well as the methods of calculation, are not available.

D. GILMAN

D. H. ROCK



W Plane
 $w = \log z$



FIG. 10

Q Plane
 $Q = \log \frac{u}{q} + i\theta$

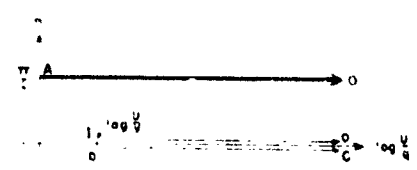


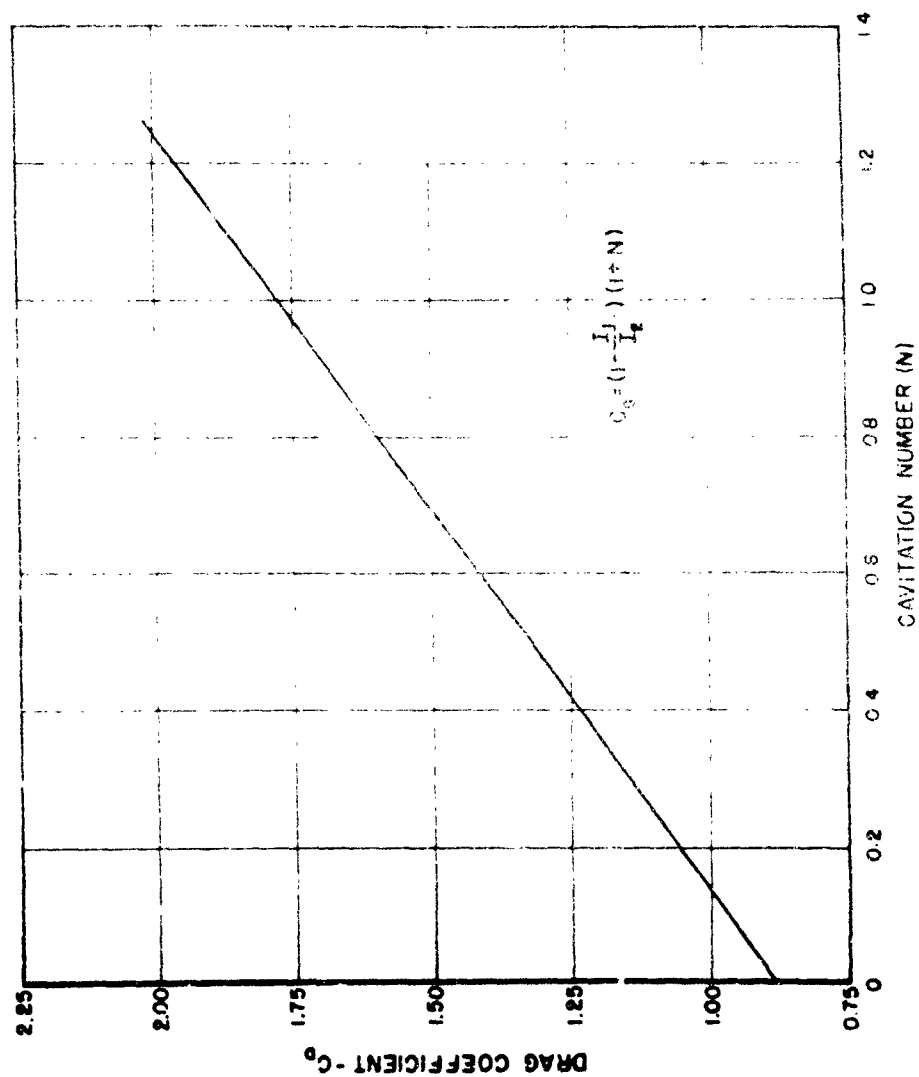
FIG. 10

ξ Plane

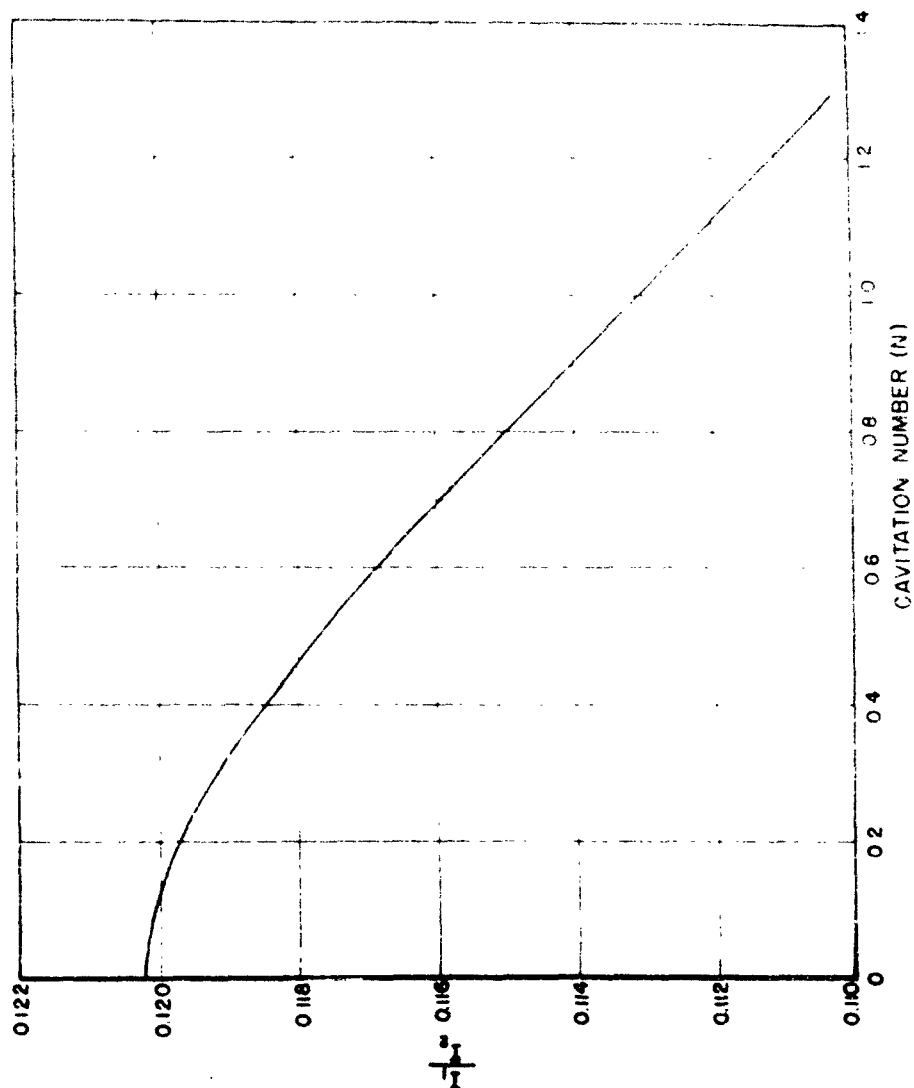


FIG. 12

NO. 8710



DRAG COEFFICIENT AS FUNCTION OF CAVITATION NUMBER



VARIATION OF I_1/I_2 WITH CAVITATION NUMBER

NOLM 8716

Z-Plane

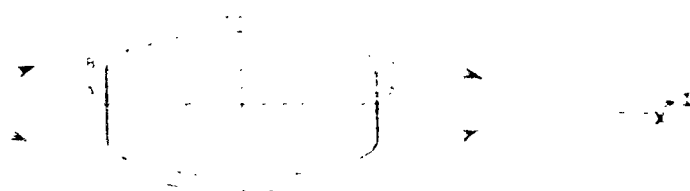


FIG. 4A

W-Plane
 $W = z^a + 1$

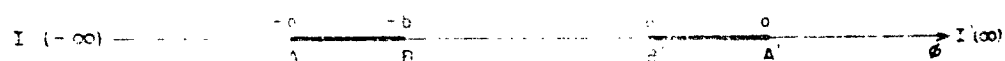


FIG. 4B

Q-Plane
 $Q = \log \frac{U}{Q} + i\theta$

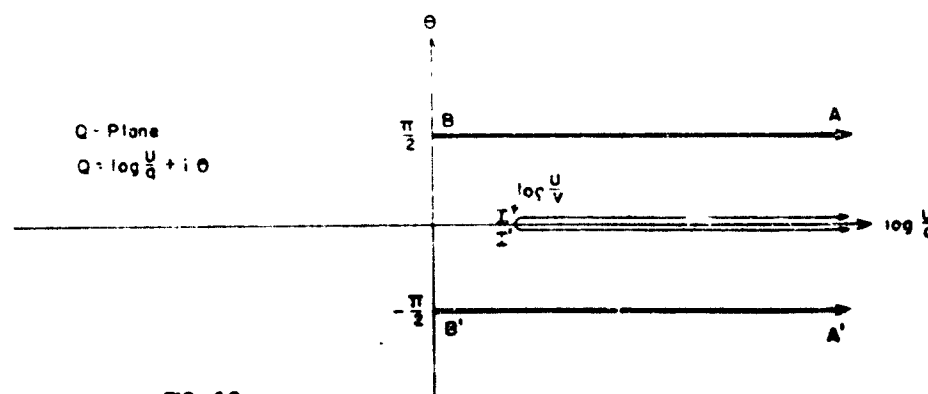


FIG. 4C

Table I

Numerical Values for the Terner Model

		I_0	I_1	I_2	I_3	I_4	I_5
0.2500		0.2500					
0.2501	0.0001	0.2501	0.4190	3.582	0.1190	0.2190	27.1
0.2504	0.0004	0.2504	0.4287	3.582	0.1197	0.2196	67.13
0.2508	0.0008	0.2508	0.4281	3.594	0.1191	0.2192	30.97
0.2513	0.0013	0.2513	0.4275	3.608	0.1185	0.2185	19.68
0.2519	0.0019	0.2519	0.4267	3.624	0.1177	0.2183	17.56
0.2553	0.0053	0.2553	0.4222	3.723	0.1154	0.2154	1.716
0.2577	0.0077	0.2577	0.4191	3.795	0.1104	0.2133	3.198

Table II

Numerical Values for the Rishboushinski Model

M	11×10^4	11×10^4	I_0/I_1	I_1/I_2	$-1 \times$ orvity length	$-1 \times$ orvity diameter
0.094	4.293	35.72	0.1202	1.001	279.1	12.97
0.196	17.14	143.2	0.1197	1.004	69.18	6.72
0.308	38.48	323.1	0.1191	1.009	30.41	4.64
0.397	59.74	504.2	0.1185	1.014	19.36	3.82
0.491	85.14	722.9	0.1178	1.020	13.41	3.28
0.604	118.8	1016.9	0.1168	1.028	9.45	2.85
0.695	148.1	1276.4	0.1160	1.035	7.48	2.62
0.794	181.3	1575.6	0.1151	1.043	6.02	2.40
0.901	218.5	1915.6	0.1141	1.052	4.92	2.24
1.004	255.4	2259.0	0.1131	1.061	4.15	2.11

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